

IN THE CLAIMS

Claims 1-26 (canceled)

Add the following claims:

-27 (new). A process for obtaining polyglycolyl urea resin from aromatic diglycinates for insulating electric conductor, in the absence of HCN polluting residues, comprising the following steps:

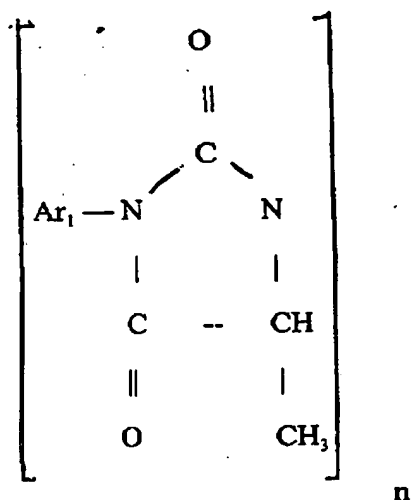
A) preparing a methyl diglycinate:

- a) reacting a mixture of methylhaloester and methylenedianiline in the presence of  $C_1-C_4$  aliphatic solvent under reflux conditions at atmospheric pressure and up to solvent reflux temperature of  $58-63^{\circ}\text{C}$ ;
- b) adding triethylamine, as catalyst at a rate of 0.178 l/hr. per Kg of reactants;
- c) separating the solvent through atmospheric distillation till 40% of its initial volume is recovered;
- d) cooling at  $20^{\circ}\text{C}$  under stirring and beginning at  $50^{\circ}\text{C}$
- e) filtering and purifying the diglycinate by washing with water;
- f) drying the methyl diglycinate obtained;

B) preparing polyglycolyl urea resin:

- a) reacting the obtained diglycinate with aromatic isocyanate in the presence of a solvent as cresylic acid in a reactor until solution is complete at 60 °C;
- b) reacting the diglycinate preferable with metilen diisocyanate solvent and catalyst at a temperature of 200°C;
- c) distilling and then cooling the reaction product; and
- d) recovering the polyglycolyl urea resin having the formula I:

I



where  $\text{Ar}_1$  is a substitute aromatic compound such as a substitute diphenylalkyl, and  $2 < n \leq 500$ .

28. (new) The process according to claim 27 wherein the methylhaloester is selected from the group consisting of methylbromopropionate and methylchloropropionate.

29. (new) The process according to claim 27 wherein the mixture reflux is conducted for at least 16 hours

30.(new) The process according to claim 27 wherein the triethylamine is added at a rate of 0.178 l/hr per Kg of product during a 3-5 hour period

31. (new) The process according to claim 27 A(h) wherein the reaction is increased up to temperature of 200°C

32. (new) The process according to claim 27 wherein the resin obtained is cooled at 70°C

33. (new) The process according to claim 27 wherein the catalyst in step (h) is selected from the group consisting of trethylenediamino and 1,4 diazobicyclo (2,2,2) octane and is added at temperatures up to 180 °C

34.(new) The process according to claim 27 wherein the polyglycolyl urea resin obtained has viscosity (Cp) of 4,800 at 15% solids.

35. (new) The process according to claim 27, wherein the C<sub>1</sub>—C<sub>4</sub> aliphatic is methanol.

36. (new) The process according to claim 27, wherein the aromatic diglycinate is preferable a methyl diglycinate obtained and is dried with hot air at 40°C and corresponds to a stereoisomer mixture with a melting point of 95 – 116°C of the following formula II:

